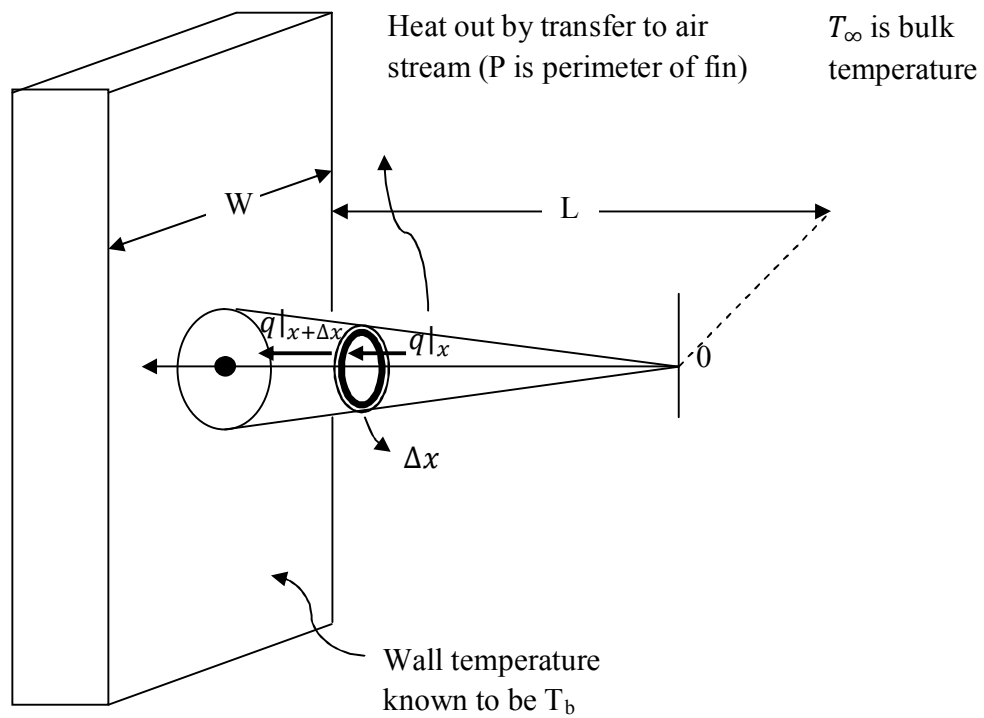


**Example 16** Heat conduction in a cooling Fin



**Figure 16** A simple cooling fin

Assume:

$$\frac{x}{L} = \frac{A_x}{A_L} = \frac{P_x}{P_L}$$

$$A_x = \frac{A_L}{L} x; P_x = \frac{P_L}{L} x$$

### Conduction heat balance around shell at steady state

[Rate of heat in] - [Rate of heat out] - [Rate of heat loss] = 0

$$q|_x \cdot A_x - q|_{x+\Delta x} \cdot A_x - h(T - T_\infty)P_x \Delta x = 0$$

Substitute  $A_x = \frac{A_L}{L}x$  and  $P_x = \frac{P_L}{L}x$  into the above equation

$$q|_x \cdot \frac{A_L}{L}x - q|_{x+\Delta x} \cdot \frac{A_L}{L}x - h(T - T_\infty) \frac{P_L}{L}x \Delta x = 0$$

Divided by  $\frac{A_L}{L} \Delta x$  through equation and taking limit  $\Delta x \rightarrow 0$  we get

$$- \lim_{\Delta x \rightarrow 0} \left( \frac{q|_{x+\Delta x} \cdot x - q|_x \cdot x}{\Delta x} \right) - h(T - T_\infty) \frac{P_L}{A_L} x = 0$$

From the definition of derivative equation we obtain

$$- \frac{d(x \cdot q_x)}{dx} - h(T - T_\infty) \frac{P_L}{A_L} x = 0$$
$$- \frac{d(x \cdot q_x)}{dx} = h(T - T_\infty) \frac{P_L}{A_L} x$$

Apply Fourier's law;

$$\frac{k}{x} \frac{d}{dx} \left( x \frac{dT}{dx} \right) = h(T - T_\infty) \frac{P_L}{A_L}$$

$$\frac{1}{x} \frac{d}{dx} \left( x \frac{dT}{dx} \right) = (T - T_\infty) \frac{P_L h}{k A_L} \quad (2)$$

Set dimensionless group:  $\theta = \frac{(T - T_\infty)}{(T_b - T_\infty)}$ ;  $dT = (T_b - T_\infty) d\theta$ , equation (2) becomes:

$$d\theta = d \left[ \frac{(T - T_\infty)}{(T_b - T_\infty)} \right]$$

$$d\theta = \frac{1}{(T_b - T_\infty)} d[(T - T_\infty)]$$

$$d\theta = \frac{1}{(T_b - T_\infty)} [dT + 0]$$

$$(T_b - T_\infty) d\theta = dT$$

$$\frac{1}{x} \frac{d}{dx} \left( x \frac{d\theta}{dx} \right) = \frac{(T - T_\infty)}{(T_b - T_\infty)} \frac{P_L h}{A_L k}$$

$$\frac{1}{x} \frac{d}{dx} \left( x \frac{d\theta}{dx} \right) = \theta \frac{P_L h}{A_L k}$$

$$\frac{d}{dx} \left( x \cdot \frac{d\theta}{dx} \right) = \theta x \frac{P_L h}{A_L k}$$

$$x \frac{d^2\theta}{dx^2} + \frac{d\theta}{dx} - \theta x \left( \frac{P_L h}{A_L k} \right) = 0$$

$$x^2 \frac{d^2\theta}{dx^2} + x \frac{d\theta}{dx} - x^2 \theta \left( \frac{P_L h}{A_L k} \right) = 0$$

Set:  $\frac{P_L h}{A_L k} = \beta^2$ ;

$$x^2 \frac{d^2\theta}{dx^2} + x \frac{d\theta}{dx} - x^2 \beta^2 \theta = 0$$

$$x^2 \frac{d^2\theta}{dx^2} + x \frac{d\theta}{dx} - (x^2\beta^2 - 0^2)\theta = 0 \quad (3)$$

From Modified Bessel:

$$x^2 \frac{d^2\theta}{dx^2} + x \frac{d\theta}{dx} - (x^2\beta^2 + n^2)\theta = 0$$

Solution

$$\theta = AI_0(\beta x) + BK_0(\beta x) \quad (4)$$

**Case I: The fin is very long, and the temperature at the end of the fin is essentially that of the surrounding fluid.**

Assume long fin;  $L \rightarrow \infty$

$$\text{BC1: } x = 0; \left. \frac{dT}{dx} \right|_{x=0} = 0; \left. \frac{d\theta}{dx} \right|_{x=0} = 0$$

$$\text{BC2: } x = L; T = T_b; \theta = 1$$

$$\frac{d\theta}{dx} = A \frac{dI_0(\beta x)}{dx} + \frac{BdK_0(\beta x)}{dx}$$

$$\frac{d\theta}{dx} = A\beta I_1(\beta x) - BK_1\beta(\beta x)$$

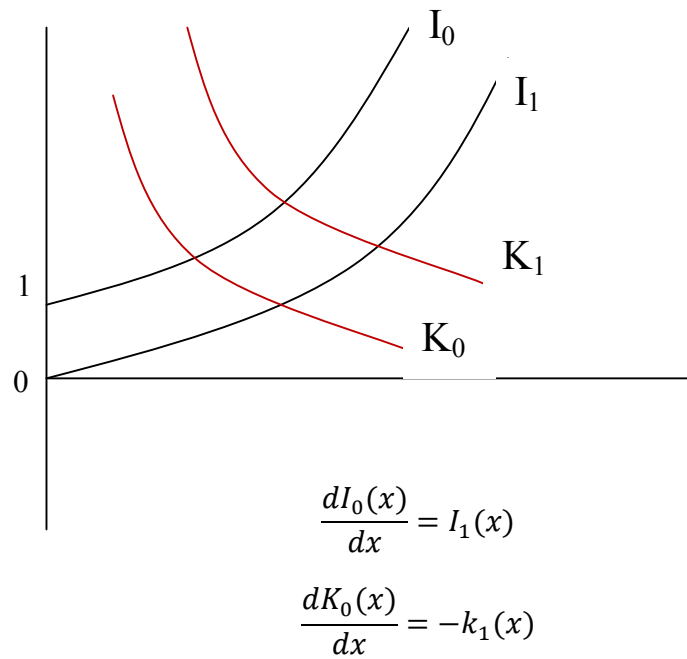
Use BC1 to substitute into eqn (3);

$$0 = AI_1(0) - BK_1(0)$$

$$\text{Finite} = \underbrace{0}_0 \quad \underbrace{\infty}_\infty$$

Because term  $K_1(0) = \infty$  and the equation is finite, we have to force  $B = 0$  to valid the equation. Eqn (4) becomes:

$$\theta = AI_0(\beta x) \quad (5)$$



Use BC2 substitute into equation (5)

$$1 = AI_0(\beta L)$$

$$A = \frac{1}{I_0(\beta L)}$$

$$\theta = \frac{I_0(\beta x)}{I_0(\beta L)}$$

Thus, we get the temperature profile:

$$T = T_\infty + (T_b - T_\infty) \frac{I_0(\beta x)}{I_0(\beta L)}; \beta = \frac{P_L h}{A_L k}$$

We can determine *heat loss* by performing derivatives with respect to x of temperature profile

$$Q_{loss} = A(-k) \left. \frac{dT}{dx} \right|_{x=L}$$

$$\left. \frac{dT}{dx} \right|_{x=L} = \frac{(T_b - T_\infty)}{I_0(\beta L)} \beta I_1(\beta x) \Big|_{x=L}$$

$$Q_{loss} = A(-k) \frac{dT}{dx} \Big|_{x=L} = \beta(T_b - T_\infty) \frac{I_1(\beta x)|_{x=L}}{I_0(\beta L)} (-k)(A_L)$$

$$Q_{loss} = -kA_L(T_b - T_\infty)\beta \frac{I_1(\beta L)}{I_0(\beta L)}$$

$$Q_{ideal} = h(T_b - T_\infty)\pi R\sqrt{R^2 + L^2}$$

$$Q_{no\ fin} = (T_b - T_\infty)\pi R_b^2$$

We can determine *fin efficiency* ( $\eta_f$ ) which is defined by

$$\eta_f = \frac{\text{actual rate of heat loss from the fin}}{\text{rate of heat loss from an isothermal fin at } T_w}$$

$$\eta_f = \frac{Q_{loss}}{Q_{ideal}}$$

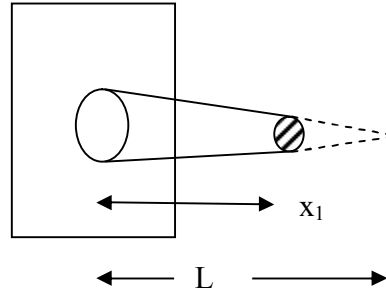
We can determine *fin effectiveness* ( $\varepsilon_f$ )

$$\varepsilon_f = \frac{Q_{actual}}{Q_{no\ fin}}$$

**Case II: The end of fin is insulated so that  $\frac{dT}{dx} = 0$  at  $x=L$  (No heat is lost from the end or from the edges.)**

$$\text{BC1: } x = x_1: \frac{dT}{dx} \Big|_{x=x_1} ; \frac{d\theta}{dx} \Big|_{x=x_1} = 0$$

$$\text{BC2: } x = L: T = T_b; \theta = 1$$



**Case III: The fin is of finite length and loses heat by convection from its end. (Facing convection BC at the tip of fin)**

$$\text{BC1: } q|_{x=x_1} = -k \frac{dT}{dx} \Big|_{x=x_1} = h(T_L - T_\infty)$$

$$-(T_b - T_\infty) \frac{d\theta}{dx} \Big|_{x=x_1} = h(T_L - T_\infty)$$

$$-k \frac{d\theta}{dx} \Big|_{x=x_1} = \frac{h(T|_{x=x_1} - T_\infty)}{T_b - T_\infty}$$

$$\frac{d\theta}{dx} \Big|_{x=x_1} = \frac{-h\theta|_{x=x_1}}{k}$$

$$\text{BC2: } x = L: T = T_b; \theta = 1$$

